

REMARKS

The specification has been amended to provide a cross-reference to the previously filed International Application. The claims have also been amended to delete improper multiple dependencies and to place the application into better form for examination.


Entry of the present amendment and favorable action on the above-identified application are earnestly solicited.

Attached hereto is a marked-up version of the changes made to the application by this Amendment.

If necessary, the Commissioner is hereby authorized in this, concurrent, and future replies, to charge payment or credit any overpayment to Deposit Account No. 02-2448 for any additional fees required under 37 C.F.R. § 1.16 or under 37 C.F.R. § 1.17; particularly, extension of time fees.

Respectfully submitted,

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Attachment: VERSION WITH MARKINGS TO SHOW CHANGES MADE

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IN THE CLAIMS:

The claims have been amended as follows:

4. (Amended) A method according to [Claims 1 to 3] Claim 1, characterized in that solid matter, such as carbonate, sulphate, and oxide of alkali metals or alkaline earth metals and/or chloride, is added to the reaction mixture to partly neutralize the solution, to bind water and/or to add nutrients to the end product.

5. (Amended) A method according to Claim 1, [2 or 4,] characterized in that the solution containing urea and phosphoric acid is the scrubber solution of a urea-based NPK process, which contains or to which has been added phosphoric acid.

6. (Amended) A method according to [Claims 1 to 5] Claim 1, characterized in that the solution containing urea and phosphoric acid is heated at 50-125 °C.

9. (Amended) A method according to Claim 6, [7 or 8,] characterized in that the solution is heated until the molar ratio of the nitrogen of the ammonia and the phosphorus of the phosphate (N/P) in the suspension is about 0.1-1.5 : 1.

10. (Amended) A method according to [Claims 1 to 9] Claim 1, characterized in preferably being continuous and diphasic: in the first phase, water is evaporated in one or more reactors at about 100 °C, until the moisture of the formed suspension is < 20% and the pH is 3-5 and, in a second phase, evaporation is continued in one or more reactors at about 110-115 °C, until the moisture of the suspension is < 10% and its pH is about 6-6.5.

11. (Amended) A method according to [Claims 1 to 10] Claim 1, characterized in that the product suspension containing ammonium phosphate and/or urea ammonium phosphate is solidified in the form of a layer of 1-30 mm, preferably 10mm in thickness, spread on a sheet-iron belt conveyor, which can be heated and/or cooled, and which is heated and/or cooled for 0.01-2 hours, preferably at a retention time of 0.05-0.5 hours to a final temperature of < 50 °C.

12. (Amended) A method according to [Claims 1 to 11] Claim 1, characterized in that the solidified end product is dried, crushed, ground and/or granulated.

13. (Amended) A solid ammonium phosphate and/or urea ammonium phosphate product, characterized in being manufactured by the method according to [any of the preceding Claims] Claim 1.

16. (Amended) A method according to Claim 3 [or 15], characterized in that the solution containing urea and phosphoric

17. (Amended) A method according to Claim 3, [15 or 16,]  
characterized in that the solution is heated until the pH of the  
suspension is 4-6.5.

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